# Modeling the removal of Arsenic by nano-scale zero valent iron

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#### Outline

- Introduction
- Mechanism
- Case study
- Objective
- Results
- Conclusion
- Future works
- References

#### Introduction

- Arsenic:
  - > One of the most toxic, naturally occurring groundwater contaminants.
  - > Sources: Natural and anthropogenic.
  - Speciation: Arsenate (As(V)) oxyanions ( $H_2AsO_4^{-1}$  and  $HAsO_4^{-2}$ ) and arsenite (As(III)) ( $H_3AsO_3$ ,  $As^{3+}$ ).
  - ➤ Health effect: Causes different types of health problems in human including cancer, uterine function damage (Akram et al., 2010), higher heart stroke rates, bladder cancer (Marshall et al., 2007)etc.
  - > WHO drinking water safety limit for As is 10μg/L.

#### Introduction

- Nano-scale zero valent iron:
  - > Size: 1 to 100 nm
  - ➤ High surface area
  - > NZVI particles are able to treat chlorinated compounds, heavy metals, dichromate and pesticides.
  - > NZVI particles and their corrosion products are suitable for remediation of both As (III) and As (V) (Kanel et al., 2005; Bezbaruah et al., 2014)

## Mechanism of As removal by NZVI:

- Adsorption
  - Formation of iron hydroxides: oxidation
    Fe(OH)2, Fe(OH)
    3, FeOOH
- Reduction
  - > NZVI core

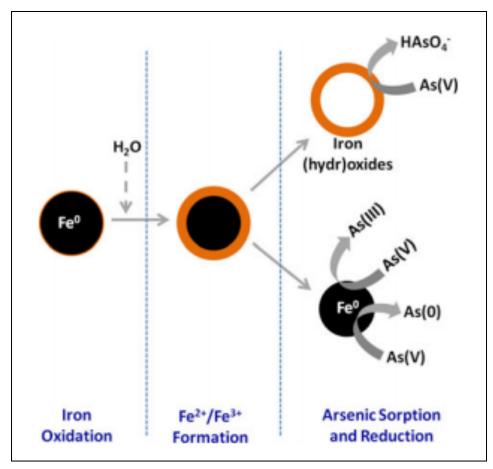


Figure. Schematic of possible mechanisms of As removal by NZVI. (Bezbaruah et al., 2014)

#### **Surface Complexation Model**

• In all surface complexation models, sorption is a function of both chemical and electrostatic energy as described by the free energy relationship:

$$\Delta Gtot = \Delta Gads + zF\psi$$

where  $\Delta G$  is the Gibbs energy (J/mol), z is the charge number (unitless) of the sorbed species, F is the Faraday constant (96,485 C/mol),  $\psi$  is the potential (V).

- PHREEQC has two models for surface complexation:
  - Dzombak and Morel,1990
  - > CD-MUSIC

#### The paper researched

• Rozell D. 2010 Modeling of removal of Arsenic by iron oxide coated sand. Journal of Environmental Engineering. 136:246-248.

## **Case Study**

#### Methodology:

- An arsenic filtration experiment using iron oxide coated sand was modeled using the USGS geochemical program PHREEQC.
- PHREEQC software uses the Dzombak and Morel (1990) model for surface complexation of iron oxide.
- Assumption:
  - Ferrichydrite or hydrous ferric oxide Hfo is the primary iron oxide surface due to its large surface area and number of binding sites.
  - > weak sites 0.2 mole/mole Hfo, 0.005 mole/mole Hfo.

# **Case Study**

## • PHREEQC input values:

Fe(OH)3	0.0336 moles
Strong binding sites	0.000168 moles
Weak binding sites	0.00671 moles
Mass	3.59
Temperature	25 degree C
рН	7.5
pe	4
As	0.00000538 moles

#### **Case Study**

• Results:

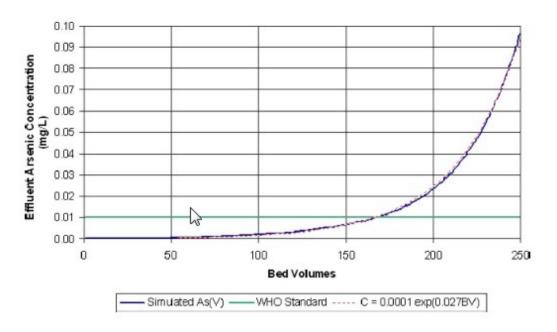


Figure. Iron oxide coated sand removal of As(V) during simulated column test

• The original experiment filtered 165 bed volumes to concentrations less than 0.01 mg/L As and approximately 210 bed volumes to 0.05 mg/L As. The model filtered 168 bed volumes to 0.01 mg/L As and 228 bed volumes to 0.05 mg/L.

## **Objective**

- To model the removal of arsenic by adsorption on surfaces of NZVI particles
- Compare with experimental results (Bezbaruah et al., 2014)

## **Modeling Procedure**

- Using PHREEQC model from USGS, the adsorption of As on iron hydroxide surface of NZVI was modeled.
- Input values used for modeling:

As(V)	0.000135 moles
NZVI	0.00855 moles
Weak sites	0.00171 moles
Strong sites	0.000043 moles
Total Hfo	0.91 gram
рН	5.0
pe	4
Temperature	25 deg C

Database: WATEQ4F

## **Modeling Procedure**

```
TITLE Example 8.--Sorption of arsenic on hydrous iron oxides layer of NZVI.
SURFACE SPECIES
     Hfo soH + H+ = Hfo soH2+
     log k 7.18
     Hfo_sOH = Hfo_sO- + H+
     10g K -8.82
     Hfo sOH + H3AsO4 = Hfo sOHAsO4-3 + 3H+
     log k -10.12
     Hfo_wOH + H+ = Hfo_wOH2+
     log k 7.18
     Hfo wOH = Hfo wO- + H+
     log k -8.82
     Hfo wOH + H3AsO4 = Hfo wHAsO4 - + H + + H2O
     log k 2.81
     Hfo wOH + H3AsO4 = Hfo wH2AsO4 + H2O
     log k 8.61
     Hfo wOH + H3AsO4 = Hfo wOHAsO4-3 + 3H+
     log k -10.12
SURFACE 1
                                      0.91
     Hfo sOH
                    4.27e-5
                               54.
     Hfo wOH
                    1.71e-3
      -donnan
END
SOLUTION 1
     -units mmol/kgw
     pН
             8.0
     As
             0.135
     Na
             100.
                     charge
     N(5)
             100.
SELECTED OUTPUT
     -file As1.35e 4
     -reset false
USER PUNCH
  10 FOR i = 5.0 to 8 STEP 0.25
  20 a$ = EOL$ + "USE solution 1" + CHR$(59) + " USE surface 1" + EOL$
  30 a$ = a$ + "EQUILIBRIUM PHASES 1" + EOL$
  40 a$ = a$ + " Fix_H+ " + STR$(-i) + " NaOH 10.0" + EOL$
  50 a = a$ + "END" + EOL$
```

	Adsorption reaction	LogK
Case 1 to -3	$H_3AsO_4 + Hfo_wOH = Hfo_wOHAsO_4^{3-} + 3H^+$	-10.12
	$H_3AsO_4 + Hfo\_sOH = Hfo\_sOHAsO_4^{3-} + 3H^+$	-10.12
Case4	$H_3AsO_4 + Hfo_wOH = Hfo_wHAsO_4^- + H^+ + H_2O$	2.81
	$H_3AsO_4 + Hfo_wOH = Hfo_wH_2AsO_4 + H_2O$	8.61
	$H_3AsO_4 + Hfo_wOH = Hfo_wOHAsO_4^{3-} + 3H^+$	-10.12
	$H_3AsO_4 + Hfo_sOH = Hfo_sOHAsO_4^{3-} + 3H^+$	-10.12

(Allison et al., 1990)

#### Initial solution

#### **Final Solution**

	501uc.	ion composic	1011			ion composi
Elements	Molality	Moles		Elements	Molality	Moles
As	1.350e-04	1.350e-04		As	7.038e-11	7.038e-11
I(5)	1.000e-01	1.000e-01		N	1.000e-01	1.000e-01
Na	1.003e-01	1.003e-01	Charge balance	Na	9.984e-02	9.984e-02

- So, 99.99 % As has been removed by the adsorption on NZVI surfaces
- Bezbaruah et al., 2014 found 99.57% removal of As with the same amount of NZVI and same initial concentration of As.

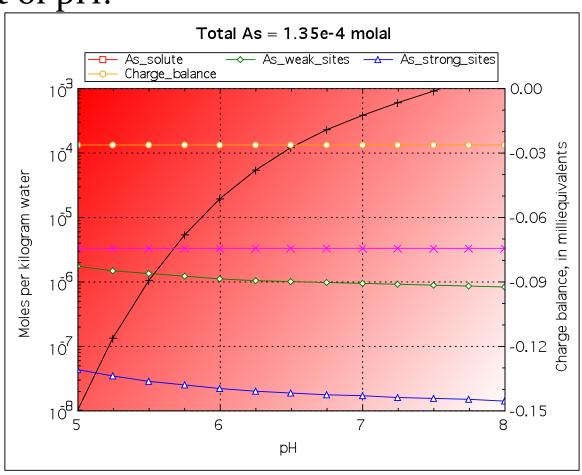
	Surfa	ce composit:	ion				
Hfo							
1.500e-04	Surface charge,	eq					
2.945e-01	sigma, C/m²						
1.423e-01	psi, V						
-5.538e+00	-F*psi/RT						
3.934e-03	exp(-F*psi/RT)						
5.400e+01	specific area, m	specific area, m²/g					
4.914e+01	m² for 9.100e-	01 g					
Hfo s							
4.270e-05	moles						
225,5-T V.T.T.0 V.F. F.		Mole		Log			
Species	Moles	Fraction	Molality				
Hfo_sOH	2.415e-05	0.565	2.415e-05	-4.617			
Mfo_son2+	1.438e 05	0.337	1.438e-05	-4.842			
Hfo_sOHAsO4-	-3 3.249e-06	0.076	3.249e-06	-5.488			
Hfo_sO-	9.290e-07	0.022	9.290e-07	-6.032			
Hfo_w							
1.710e-03	moles	Mole		7			
Charias	Moles	Fraction	Walalite	Log			
Species	noies	Fraction	Molality	Molality			
Hfo wOH	9.660e-04	0.565	9.660e-04	-3.015			
Hfo wOH2+	5.751e-04	0.336	5.751e-04	-3.240			
Hfo_wOHAsO4-	-3 1.300e-04	0 076	1.300e-04	-3.886			
Hfo_wO-	3.717e-05	0.022	3.717e-05	-4.430			
Hfo_wHAsO4-	1.718e-06	0.001	1.718e-06	-5.765			
Hfo_wH2AsO4	4.264e-08	0.000	4.264e-08	-7.370			
Hfo wH2AsO3	3.910e-32	0.000	3.910e-32	-31.408			

#### **Initial Solution**

#### Final Solution

Log   Log   Camma   Cam   Species   Molality   Activity   Gamma   Cam   Species   Molality   Activity   Molality   Activity   Gamma   Cam   Species   Molality   Activity   Molality   Activity   Molality   Activity   Gamma   Cam   Species   Molality   Activity   Molality   Activity   Molality   Activity   Gamma   Cam   Species   Molality   Activity   Molality   Activity   Molality   Activity   Gamma   Cam   Species   Molality   Activity   Molality   Activity   Gamma   Cam   Species   Molality   Activity   Molality   Activity   Molality   Activity   Gamma   Cam   Species   Molality   Activity   Gamma   Cam   Species   Molality   Activity   Molality   Activity   Gamma   Cam   Species   Molality   Activity   Gamma   Cam   Cam	mole cm³/m 0. (0) 18. (0) (0) (0)
OR-	(0) 10. (0) (0)
H+ 1.212e-08 1.000e-08 -7.917 -8.000 -0.083	(0) (0)
H2O	(O) (O)
AS (3) 3.248e-16 H3AsO3 2.973e-16 3.042e-16 -15.527 -15.517 0.010 H2AsO3- 1.422e-38 1.111e-38 -37.847 -37.954 -0.107 H2AsO3- 2.758e-17 2.154e-17 -16.559 -16.667 -0.107 H2AsO3+ 9.952e-40 7.775e-40 -39.002 -39.109 -0.107 HASO3-2 1.155e-23 4.297e-24 -22.937 -23.367 -0.429 H2AsO3- 0.000e+00 0.000e+00 -47.225 -47.654 -0.422 H4AsO3+ 1.930e-24 1.507e-24 -23.714 -23.822 -0.107 AsO3-3 0.000e+00 0.000e+00 -57.389 -58.354 -0.965 AsO3-3 7.932e-31 8.574e-32 -30.101 -31.067 -0.966 AsO3-3 0.000e+00 0.000e+00 -57.389 -58.354 -0.965 As(5) 1.350e-04 H2AsO4- 6.927e-11 5.412e-11 1.01.159 -10.267 -0.107 H2AsO4- 8.690e-06 6.787e-06 -5.061 -5.168 -0.107 H3AsO4 1.055e-12 3.744e-13 -11.998 -12.427 -0.422 H2AsO4- 8.690e-06 6.787e-06 -5.061 -5.168 -0.107 H3AsO4 1.055e-13 1.080e-13 -12.977 -12.967 0.010 AsO4-3 9.725e-08 1.051e-08 -7.012 -7.978 -0.966 AsO4-3 7.731e-19 8.382e-20 -18.112 -19.077 -0.965 H3AsO4 1.323e-11 1.354e-11 -10.878 -10.868 0.010 H(0) 0.000e+00 HO 0.000e+00	(0)
H3As03 2.973e-16 3.042e-16 -15.527 -15.517 0.010 H2As03 1.33e-34 1.36e-34 -37.847 -37.954 0.107 H2As03- 2.758e-17 2.154e-17 -16.559 -16.667 -0.107 H4As03+ 9.952e-40 7.775e-40 -39.002 -39.109 -0.107 H4As03+ 1.930e-24 1.507e-24 -22.937 -23.367 -0.429 HAs03-2 0.000e+00 0.000e+00 -47.225 -47.654 -0.425 H2As03- 3.7932e-31 8.574e-32 -30.101 -31.067 -0.966 As(5) 7.038e-11	(0)
H2As03- 2.758e-17 2.154e-17 -16.559 -16.667 -0.107 H4As03+ 9.952e-40 7.775e-40 -39.002 -39.109 -0.107 H4As03+ 1.930e-24 1.557e-24 -22.937 -23.367 -0.429 HAs03-2 0.000e+00 0.000e+00 -47.225 -47.654 -0.429 HAs03-3 0.000e+00 0.000e+00 -57.389 -58.354 -0.965 As03-3 7.932e-31 8.574e-32 -30.101 -31.067 -0.966 As03-3 0.000e+00 0.000e+00 -57.389 -58.354 -0.965 As(5) 7.038e-11	2000
HASO3-2 1.155e-23 4.297e-24 -22.937 -23.367 -0.429 HASO3-2 0.000e+00 0.000e+00 -47.225 -47.654 -0.429 HASO3-3 0.000e+00 0.000e+00 -57.389 -58.354 -0.965 ASO3-3 7.932e-31 8.574e-32 -30.101 -31.067 -0.966 AS(5) 7.038e-11	(0)
H4AsO3+ 1.930e-24 1.507e-24 -23.714 -23.822 -0.107 AsO3-3 0.000e+00 0.000e+00 -57.389 -58.354 -0.965 AsO3-3 7.932e-31 8.574e-32 -30.101 -31.067 -0.966 As(5) 7.038e-11	
ABOST 7.932e-31 8.574e-32 -30.101 -31.067 -0.966 AB (5) 7.038e-11  HABO4-2 1.262e-04 4.695e-05 -3.899 -4.328 -0.429 HABO4-2 1.005e-12 3.744e-13 -11.998 -12.427 -0.429 H2ABO4- 8.690e-06 6.787e-06 -5.061 -5.168 -0.107 H3ABO4 1.055e-13 1.080e-13 -12.977 -12.967 0.016 ABO4-3 9.725e-08 1.051e-08 -7.012 -7.978 -0.966 ABO4-3 7.731e-19 8.382e-20 -18.112 -19.077 -0.965 H3ABO4 1.323e-11 1.354e-11 -10.878 -10.868 0.010 H(0) 0.000e+00	(0)
H2AsO4- 6.927e-11 5.412e-11 10.159 -10.267 -0.107  HAsO4-2 1.262e-04 4.695e-05 -3.899 -4.328 -0.429 HAsO4-2 1.005e-12 3.744e-13 -11.998 -12.427 -0.429  H2AsO4- 8.690e-06 6.787e-06 -5.061 -5.168 -0.107 H3AsO4 1.055e-13 1.080e-13 -12.977 -12.967 0.016  AsO4-3 9.725e-08 1.051e-08 -7.012 -7.978 -0.966 AsO4-3 7.731e-19 8.382e-20 -18.112 -19.077 -0.965  H3AsO4 1.323e-11 1.354e-11 -10.878 -10.868 0.010 H(0) 0.000e+00  H2 0.000e+00 0.000e+00 0.000e+00 -43.349 -43.339 0.016  H2 0.000e+00 0.000e+00 0.000e+00 -52.691 -52.798 -0.107  NO3- 1.000e-01 7.531e-02 -1.000 -1.123 -0.123 NH3 0.000e+00 0.000e+00 -57.042 -57.042 0.000  NO3- 1.003e-01 N(0) 1.543e-06	(0)
HASO4-2 1.262e-04 4.695e-05 -3.899 -4.328 -0.429 HASO4-2 1.005e-12 3.744e-13 -11.998 -12.427 -0.425 H2AsO4- 8.690e-06 6.787e-06 -5.061 -5.168 -0.107 H3AsO4 1.055e-13 1.080e-13 -12.977 -12.967 0.010 AsO4-3 9.725e-08 1.051e-08 -7.012 -7.978 -0.966 AsO4-3 7.731e-19 8.382e-20 -18.112 -19.077 -0.965 H3AsO4 1.323e-11 1.354e-11 -10.878 -10.868 0.010 H(0) 0.000e+00	
H2AsO4- 8.690e-06 6.787e-06 -5.061 -5.168 -0.107 H3AsO4 1.055e-13 1.080e-13 -12.977 -12.967 0.010 AsO4-3 9.725e-08 1.051e-08 -7.012 -7.978 -0.966 AsO4-3 7.731e-19 8.382e-20 -18.112 -19.077 -0.965 H3AsO4 1.323e-11 1.354e-11 -10.878 -10.868 0.010 H(0) 0.000e+00  (0) 1.384e-27	(0)
ASO4-3 9.725e-08 1.051e-08 -7.012 -7.978 -0.966 ASO4-3 7.731e-19 8.382e-20 -18.112 -19.077 -0.965 H3AsO4 1.323e-11 1.354e-11 -10.878 -10.868 0.010 H(0) 0.000e+00	(0)
H3AsO4 1.323e-11 1.354e-11 -10.878 -10.868 0.010 H(0) 0.000e+00	(0)
H2 0.000e+00 0.000e+00 -43.349 -43.339 0.010 H2 6.918e-28 7.079e-28 -27.160 -27.150 0.010 N(-3) 0.000e+00 U(5) 1.000e-01	(0)
H2 6.918e-28 7.079e-28 -27.160 -27.150 0.010 N(-3) 0.000e+00 N(5) 1.000e-01 NH4+ 0.000e+00 0.000e+00 -52.691 -52.798 -0.107 NO3- 1.000e-01 7.531e-02 -1.000 -1.123 -0.123 NH3 0.000e+00 0.000e+00 -57.042 -57.042 0.000 N(0) 1.543e-06	
NH4+ 0.000e+00 0.000e+00 -52.691 -52.798 -0.107 NO3- 1.000e-01 7.531e-02 -1.000 -1.123 -0.123 NH3 0.000e+00 0.000e+00 -57.042 -57.042 0.000 NO3- 1.003e-01 N(0) 1.543e-06	(0)
NO3- 1.000e-01 7.531e-02 -1.000 -1.123 -0.123 NH3 0.000e+00 0.000e+00 -57.042 -57.042 0.000  N(0) 1.543e-06  N(0) 1.543e-06	
N(0) 1.543e-06  N(0) 1.543e-06	(0)
1.003E-01	(0)
No. 1 0020 01 7 9450 02 0 000 1 105 0 107 N2 7.716e-07 7.895e-07 -6.113 -6.103 0.010	
	(0)
N(3) 2.326e-13	
O2 8.072e-39 8.261e-39 -38.093 -38.083 0.010 NO2- 2.326e-13 1.817e-13 -12.633 -12.741 -0.107	(0)
N(5) 1.000e-01	
NO3- 1.000e-01 7.535e-02 -1.000 -1.123 -0.123	(0)
Na 9.984e-02	
Na+ 9.984e-02 7.814e-02 -1.001 -1.107 -0.106	(0)
O(0) 3.858e-06	
02 1.929e-06 1.974e-06 -5.715 -5.705 0.010	(0)

• Effect of pH:



## • Effect of pH:

рН	Final As concentration(molality)
5.0	7.043e-11
6.0	3.805e-10
7.0	6.062e-09
8.0	3.204e-07

#### **Conclusion**

- The model yeilded 99.99% removal of arsenic by NZVI whereas the experimental results yielded 99.57% removal of arsenic by NZVI
- Removal efficiency decreases with the increase of pH.
- More realistic results can be found by using the real K values for NZVI, sample of groundwater and also by incorporating reduction process in the model.

#### References

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